

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions and listings of claims in the application:

LISTING OF CLAIMS:

1. (currently amended): A method for producing a purified 2-cyanoacrylate by distilling a crude 2-cyanoacrylate in the presence of a polymerization inhibitor, characterized in that a an anionic polymerization inhibitor having a boiling point at normal pressure of within $\pm 12^{\circ}\text{C}$ of the boiling point at normal pressure of the purified 2-cyanoacrylate is used as the polymerization inhibitor,

wherein the anionic polymerization inhibitor is a halocarboxylic acid, a halosulfonic acid, a BF_3 methanol complex or a BF_3 ethanol complex, and

wherein distillation is carried out by further adding, to a 2-cyanoacrylate in a vessel, an anionic polymerization inhibitor having a boiling point that is higher than the boiling point of the 2-cyanoacrylate by more than 12°C and a radical polymerization inhibitor having a boiling point that is higher than the boiling point of the 2-cyanoacrylate by more than 12°C .

2. (canceled).

3. (currently amended): The production method according to claim 2, wherein the anionic polymerization inhibitor is a halocarboxylic acid or a halosulfonic acid.

4. (original): The production method according to claim 3, wherein the halocarboxylic acid or the halosulfonic acid is chloroacetic acid, dichloroacetic acid, trichloroacetic acid, bromoacetic acid, dibromofluoroacetic acid, 3-chloropropionic acid, 2,2-dichloropropionic acid, 2-bromopropionic acid, 2-chlorobutyric acid, 4-chlorobutyric acid, pentafluoropropanesulfonic

acid, nonafluorobutanesulfonic acid, trichloroacrylic acid, undecafluoropentanesulfonic acid, tridecafluorohexanesulfonic acid, or 3-methylsulfanylpropionic acid.

5. (currently amended): The production method according to claim 2 claim 1, wherein the anionic polymerization inhibitor is a BF_3 methanol complex or a BF_3 ethanol complex.

6. (original): The production method according to claim 1, wherein the polymerization inhibitor is added to a vessel in advance.

7. (original): The production method according to claim 1, wherein the polymerization inhibitor is dissolved in a purified 2-cyanoacrylate and continuously added via an upper part of a distillation vessel or an upper part of a distillation column.

8. (original): The production method according to claim 6, wherein the polymerization inhibitor is added at 1 to 1000 wt ppm relative to the crude 2-cyanoacrylate.

9. (original): The production method according to claim 7, wherein the polymerization inhibitor is added at 1 to 1000 wt ppm relative to the crude 2-cyanoacrylate.

10. (previously presented): The production method according to claim 1, wherein a crude 2-cyanoacrylate obtained by heating and condensing a cyanoacetic acid ester and formaldehyde in an organic solvent in the presence of a basic catalyst, and depolymerizing the condensate thus obtained in the presence of a depolymerization catalyst and a polymerization inhibitor at reduced pressure and high temperature is used as the crude 2-cyanoacrylate.

11. (previously presented): The production method according to claim 1, wherein distillation employs a method in which heating is carried out at reduced pressure using a packed distillation column.

12. (canceled).

13. (currently amended): The production method according to ~~claim 12~~ claim 1, wherein the anionic polymerization inhibitor having a boiling point that is higher than the boiling point of the 2-cyanoacrylate by more than 12°C is phosphorus pentoxide and the radical polymerization inhibitor having a boiling point that is higher than the boiling point of the 2-cyanoacrylate by more than 12°C is hydroquinone.